

In the Claims:

Please amend the claims as follows.

1. (previously presented) A middle distillate selective hydrocracking catalyst composition which comprises a metal hydrogenation component selected from the group of metals consisting of molybdenum, tungsten, cobalt, nickel and combinations of two or more thereof supported on a carrier comprising an amorphous binder component and from 2 to 80% by weight, based on the total weight of the carrier, a zeolite of the faujasite structure having a unit cell size in the range of from 24.14 to 24.38 Å, a bulk silica to alumina ratio (SAR) above about 12, and a surface area of at least about 850 m²/g as measured by the BET method and ATSM D 4365-95 with nitrogen adsorption at a p/po value of 0.03, and a micropore volume of at least about 0.28 ml/g.
2. (previously presented) A composition as claimed in claim 1, wherein the zeolite has a unit cell size in the range of from 24.24 to 24.38 Å.
3. (original) A composition as claimed in claim 1, wherein the zeolite has a SAR in the range of from about 20 to about 100.
4. (original) A composition as claimed in claim 1, wherein the zeolite has a surface area of at least about 890 m²/g.
5. (previously presented) A composition as claimed in claim 1, wherein the zeolite has a micropore volume greater than 0.30 ml/g.
6. (original) A composition as claimed in claim 1, which further comprises a second zeolite.
7. (original) A composition as claimed in claim 6, which further comprises in the range of from 1 to 5 % by weight of zeolite beta, basis total carrier.

Claim 8 (canceled).

9. (currently amended) A hydrocracking catalyst composition of any one of claims 1, 2, 3, 4, 5, 6, and 7, which comprises a metal hydrogenation component selected from the group of metals consisting of molybdenum, tungsten, cobalt, nickel and combinations of two or more thereof supported on a carrier comprising a high surface area zeolite of the faujasite structure, wherein said high surface area zeolite is made by a process which comprises

- a) hydrothermally treating a starting zeolite of the faujasite structure having a silica to alumina molar ratio in the range of from about 4.5 to about 6.5, and an alkali content

of less than about 1.5 %wt; at a temperature in the range of from 600°C to 800°C, and at a partial pressure of steam in the range of from about 0.2 to about 1 atmosphere for a time effective to produce an intermediate zeolite having a unit cell size of from 24.30 to 24.45 Å;

b) contacting said intermediate zeolite with an acidified solution comprising an acid and an ammonium salt under conditions effective to produce said ~~high surface area~~ zeolite ~~having a unit cell size in the range of from 24.10 to 24.40 Å, a molar silica to alumina ratio of greater than about 12 and a surface area of greater than about 850 m²/g thereby producing the high surface area zeolite;~~ and

c) recovering said ~~high surface area~~ zeolite.

10. (previously presented) A process for the conversion of a hydrocarbonaceous feedstock into lower boiling materials, which comprises contacting the feedstock with hydrogen at elevated temperature and pressure in the presence of a hydrocracking catalyst composition which comprises a metal hydrogenation component selected from the group of metals consisting of molybdenum, tungsten, cobalt, nickel and combinations of two or more thereof supported on a carrier comprising an amorphous binder component and from 2 to 80% by weight, based on the total weight of the carrier, a zeolite of the faujasite structure having a unit cell size in the range of from 24.14 to 24.38 Å, a bulk silica to alumina ratio (SAR) above about 12, and a surface area of at least about 850 m²/g as measured by the BET method and ATSM D 4365-95 with nitrogen adsorption at a p/po value of 0.03, and a micropore volume of at least about 0.28 ml/g.

11. (original) A process as claimed in claim 10, which is carried out at a temperature in the range of from 250 to 500°C and a total pressure in the range of from 3×10^6 to 3×10^7 Pa.

12. (previously presented) A composition comprising:
a first zeolite of the faujasite structure having a first zeolite unit cell size in the range of from 24.24 to 24.38 Å; a bulk silica to alumina molar ratio in the range of from 20 to 100; and a surface area of at least 850 m²/g.

13. (previously presented) A composition as recited in claim 12, further comprising:
a metal hydrogenation component selected from the group consisting of nickel, cobalt, molybdenum, tungsten, platinum and palladium.

14. (previously presented) A composition as recited in claim 13, further comprising:
a second zeolite selected from the group consisting of zeolite beta, ZSM-5 and zeolite Y having a second zeolite unit cell size greater than 24.40 Å.

15. (previously presented) A composition as recited in claim 14, further comprising: an amorphous binder component selected from the group consisting of alumina, silica, silica-alumina, and mixtures thereof.

16. (previously presented) A composition as recited in claim 15, wherein said first zeolite is present in said composition in amount up to 90 weight percent and said second zeolite is present in said composition in an amount up to 20 weight percent, wherein said weight percents are based on the total sum weight of said amorphous binder component, said first zeolite and said second zeolite; and wherein said metal hydrogenation component is present in said composition in the range of from 2 to 40 parts by weight (calculated as metal) per 100 parts by weight of the total composition.

17. (currently amended) A middle distillate selective hydrocracking process, comprising: providing a feedstock comprising hydrocarbons boiling in the range of from 330 °C to 650 °C; contacting said feedstock in the presence of hydrogen at an elevated temperature and an elevated pressure with a middle distillate selective hydrocracking catalyst composition as defined in any one of claims 1, 2, 3, 4, 5, 6, 7, 23, 24, 25, 26, 27, 28, 29 and 30~~comprising a first zeolite of the faujasite structure having a first zeolite unit cell size in the range of from 24.10 to 24.40 Å; a bulk silica to alumina molar ratio in the range of greater than 12; and a surface area of at least 850 m²/g; and~~ yielding a middle distillate product comprising middle distillate hydrocarbons boiling in the range of from 150 °C to 370 °C, wherein said elevated temperature is in the range of from 250 °C to 500 °C; said elevated pressure is in the range of from 3x10⁶ to 3x10⁷ Pa; and said hydrogen is present in an amount such that the hydrogen partial pressure is in the range of from 4x10⁶ to 2.5x10⁷ Pa; and the space velocity is in the range of from 0.1 to 10 kg of said feedstock per liter of said middle distillate selective hydrocracking catalyst composition per hour (kg x l⁻¹ x hr⁻¹).

Claims 18-22 (canceled).

23. (currently amended) A middle distillate selective hydrocracking catalyst composition as recited in claim 91, wherein said unit cell size of said ~~high surface area~~ zeolite is in the range of from 24.24 to 24.38 Å and said bulk silica to alumina ratio is in the range of from 20 to 100.

24. (currently amended) A middle distillate selective hydrocracking catalyst composition as recited in claim 23, wherein said

metal hydrogenation component includes at least two hydrogenation components with a first hydrogenation component selected from the group consisting of nickel, cobalt, molybdenum[[],] and tungsten, platinum and palladium and a second hydrogenation component selected from the group consisting of nickel and cobalt.

25. (currently amended) A middle distillate selective hydrocracking catalyst composition as recited in claim 24, further comprising:

a second zeolite selected from the group consisting of zeolite beta, ZSM-5 and zeolite Y having a second zeolite unit cell size greater than 24.40 Å.

26. (currently amended) A middle distillate selective hydrocracking catalyst composition as recited in claim 25, wherein said~~and~~further comprising:

an amorphous binder component is selected from the group consisting of alumina, silica, silica-alumina, and mixtures thereof.

27. (currently amended) A middle distillate selective hydrocracking catalyst composition as recited in claim 26, wherein said ~~high surface area~~ zeolite is present in said composition in amount up to 90 weight percent and said second zeolite is present in said composition in an amount up to 20 weight percent, wherein said weight percents are based on the total sum weight of said amorphous binder component, said high surface area zeolite and said second zeolite; and wherein said metal hydrogenation component is present in said composition in the range of from 2 to 40 parts by weight (calculated as metal) per 100 parts by weight of the total composition.

28. (currently amended) A hydrotreating middle distillate selective hydrocracking catalyst composition as recited in claim 91, wherein said ~~starting~~ zeolite has a unit cell size is in the range of from 24.6024.30 to 24.7824.36 Å.

29. (currently amended) A hydrotreating middle distillate selective hydrocracking catalyst composition as recited in claim 281, wherein said unit cell size of ~~said~~ intermediate ~~zeolite~~ is in the range of from 24.3524.30 to 24.4524.35 Å.

30. (currently amended) A hydrotreating middle distillate selective hydrocracking catalyst composition as recited in claim 291, wherein said zeolite has an alkali content of ~~said~~ starting ~~zeolite is~~ less than about 1 % wt.

Please add the following new claims.

31. (new) A composition as recited in claim 12, wherein said first zeolite unit cell size is in the range of from 24.24 to 24.36.

32. (new) A composition as recited in claim 12, wherein said first zeolite unit cell size is in the range of from 24.30 to 24.35.

33. (new) A composition as recited in any one of claims 12, 31, and 32, wherein said surface area is at least 875 m²/g.

34. (new) A composition as recited in claim 12, 31, 32 and 33, wherein said first zeolite has a first zeolite micropore volume greater than about 0.28 m³/g.

35. (new) A composition as recited in claim 12, 31, 32 and 33, wherein said bulk silica to alumina molar ratio is in the range of from 20 to 50.

36. (new) A composition as recited in claim 12, 31, 32 and 33, wherein said first zeolite is made by a process that comprises:

- a) hydrothermally treating a starting zeolite of the faujasite structure having a silica to alumina molar ratio in the range of from about 4.5 to about 6.5, and an alkali content of less than about 1.5 %wt; at a temperature in the range of from 600°C to 800°C, and at a partial pressure of steam in the range of from about 0.2 to about 1 atmosphere for a time effective to produce an intermediate zeolite having a unit cell size of from 24.30 to 24.45 Å;
- b) contacting said intermediate zeolite with an acidified solution comprising an acid and an ammonium salt under conditions effective to produce said first zeolite; and
- c) recovering said first zeolite.

37. (new) A composition as recited in claim 12, wherein said first zeolite has a micropore volume of greater than about 0.28 m²/g and said first zeolite unit cell size is in the range of from 24.30 to 24.35, said bulk silica to alumina molar ratio is in the range of from 20 to 50, and said surface area is at least 910 m²/g.